



DESALINATION OF CONTAMINATED WATER VIA CLATHRATE HYDRATES

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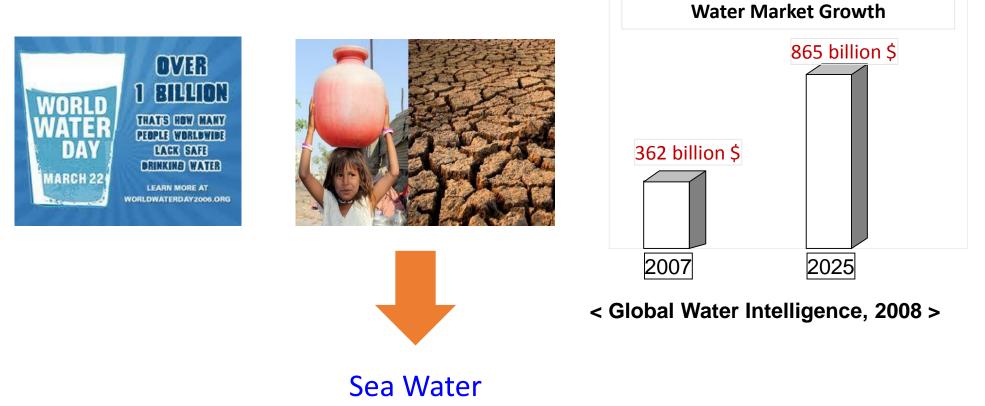


Outline

- Current Water Situation
- Existing Desalination Technologies
- Desalination via Clathrate Hydrate
- Challenges with Desalination via Clathrate Hydrate
- Thermodynamics
- Kinetics
- Conclusion and Recommendations



Current Water Situation



Abundant resource for fresh water on earth



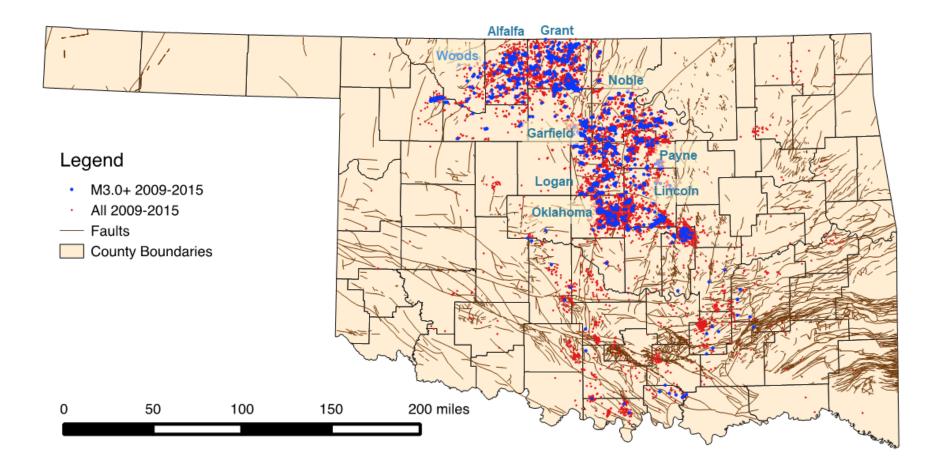
Major Water using industries

- Oil and Gas
- Petrochemical
- Power
- Food processing
- Pharmaceutical
- Microelectronics
- Pulp and paper
- Mining

Produced water (PW)

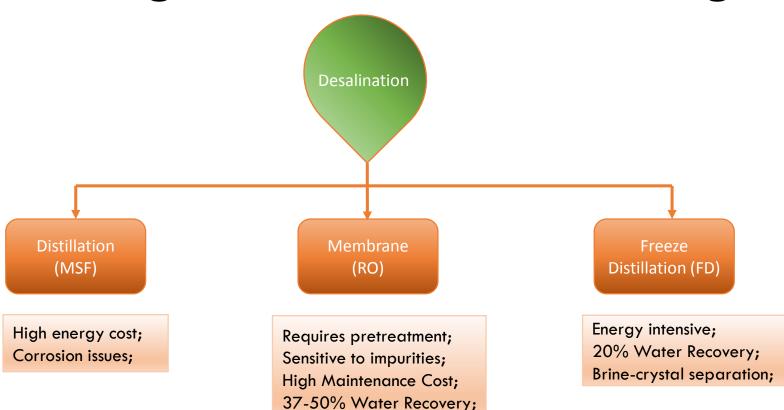
- The water found in the same formations as oil and gas and is a byproduct of oil and gas exploration and production
- PW generated throughout the World is up to 39.5 million m³ per day
- 9.2 million m³/day of produced water in US alone
- Total dissolved solids of PW can be up to 300,000 mg/L
- Treated PW can be reused for
 - irrigation,
 - livestock watering
 - aquifer storage
 - municipal and industrial uses





Jeremy Boak., "Oklahoma Earthquakes and Injection of Produced Water" Oklahoma Geological Survey, 2016

Existing Desalination Technologies



Limitations of Existing Techniques

Sensitive to salt concentration and impurities

Energy intensive



Low water recovery



Disruptive – Innovative Technologies

Disruptive – Innovative Technology

- Cost effective
- Environmentally friendly
- Low in energy consumption
- Raw material availability
- High recovery
- Sustainable

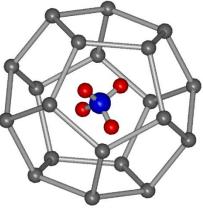


Can hydrate based desalination be the answer?



Gas hydrates are crystals like ice

- Non-stoichiometric crystalline compounds
- Formed by enclathration of guest molecules by cages formed by water molecules
- Guest molecule may be H₂, CO₂, Hydrocarbons, N₂ etc.
- Hydrates are relevant to flow assurance, energy recovery and innovative applications

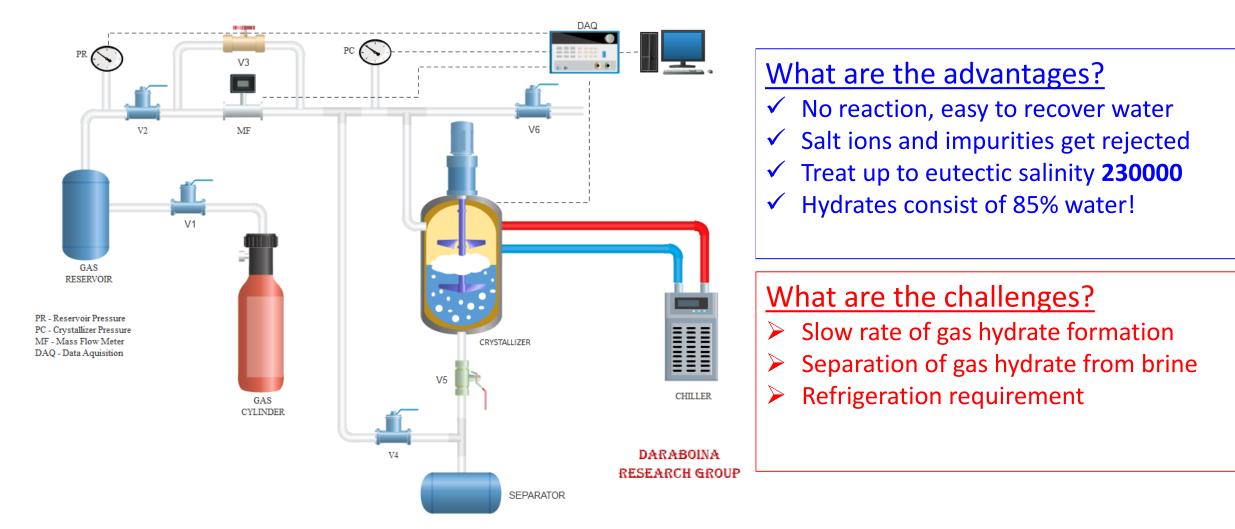


Molecular view



Naked eye view

Desalination via Clathrate Hydrate

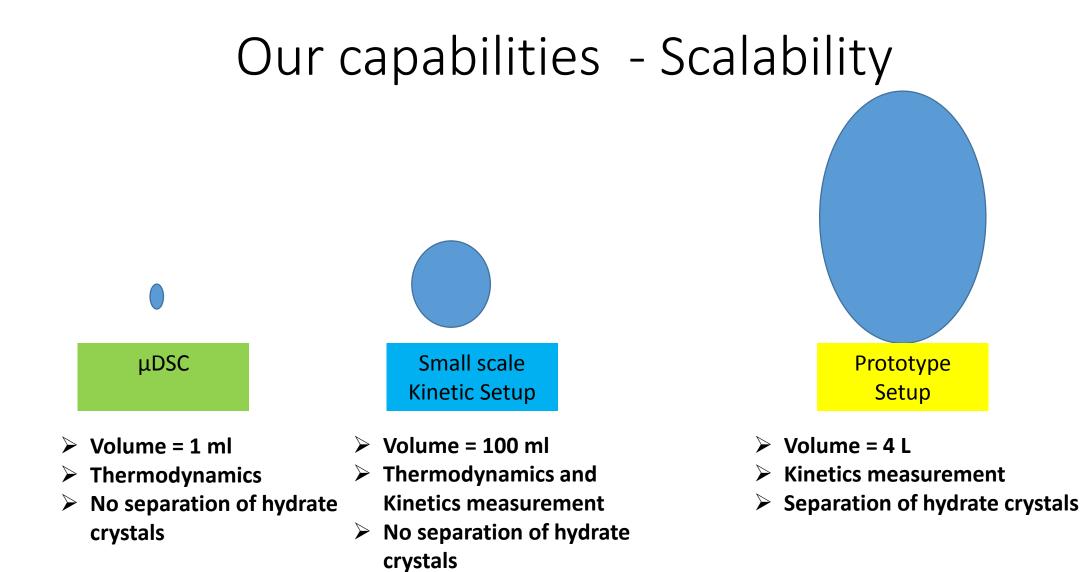




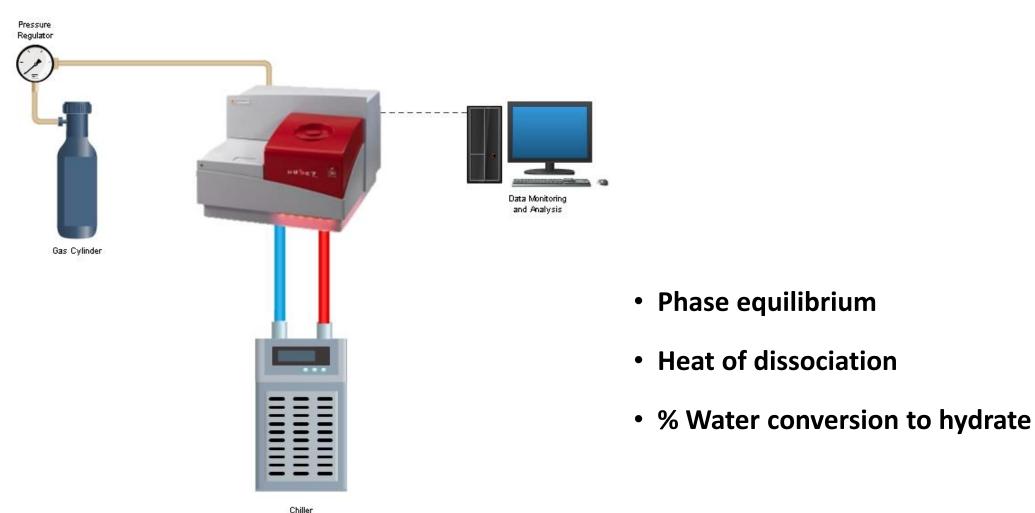
Challenges

- Refrigeration requirement ----> Thermodynamics ----> Identification of suitable hydrate former to operate at higher temperature
- Slow rate of gas hydrate formation ----> Reactor design and Suitable hydrate former
- Separation of gas hydrate from brine ----> Reactor design



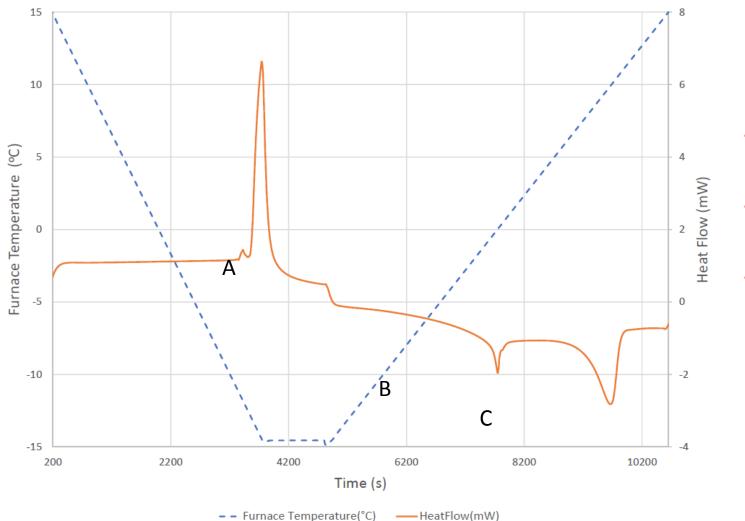


Micro Differential Scanning Calorimeter (DSC)





DSC Operating Procedure



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Research

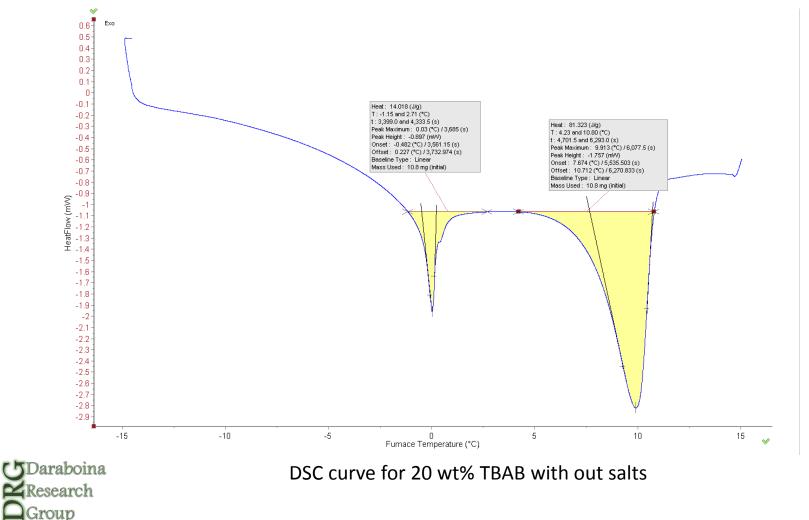
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- Cool from 15 °C to -15 °C
- Hold temperature constant

• Heat back up to 15 °C

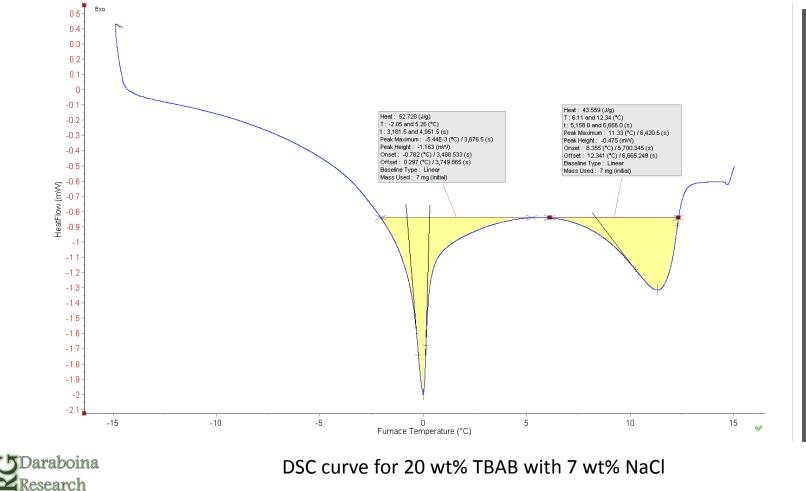
A. Formation Peak B. Ice Melting Peak C. Hydrate Melting Peak

Water Conversion Calculation



- ΔH_{Water} = 333.78 J/g
- $\Delta H_{ICE} = 14.018 \text{ J/g}$
- $\Delta H_{Hydrate} = 81.323 \text{ J/g}$
- Sample W = 10.8mg
- $\Delta H_{ICE} = 0.1514 \text{ J/Sample}$
- W_{ICE} = 0.4536mg
- W_{Hydrate} = 10.346mg
- Conversion = 95.8%

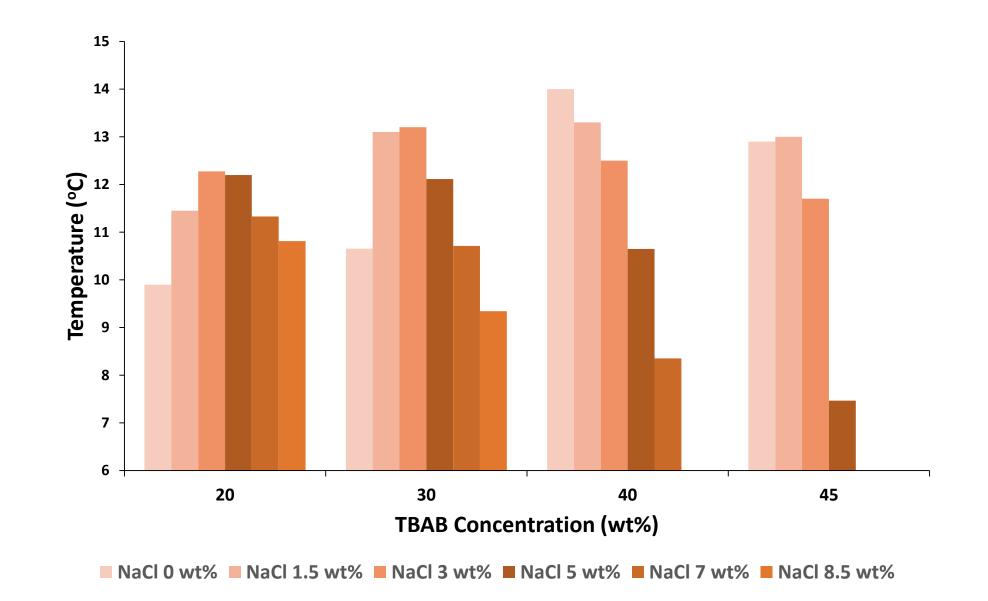
Water Conversion Calculation



Group

- $\Delta H_{Water} = 333.78 \text{ J/g}$
- ΔH_{ICE} = 52.728 J/g
- $\Delta H_{Hydrate} = 43.559 \text{ J/g}$
- Sample W = 7mg
- $\Delta H_{ICE} = 0.369 \text{ J/Sample}$
- W_{ICE} = 1.1058mg
- W_{Hydrate} = 5.894mg
- Conversion = 84.2%

Phase Equilibrium curve

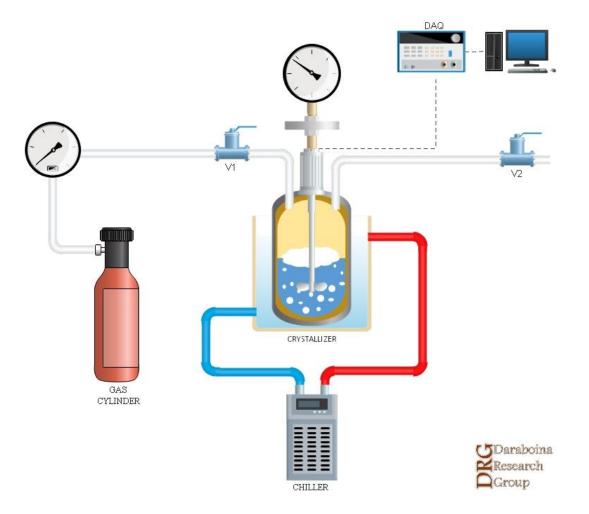


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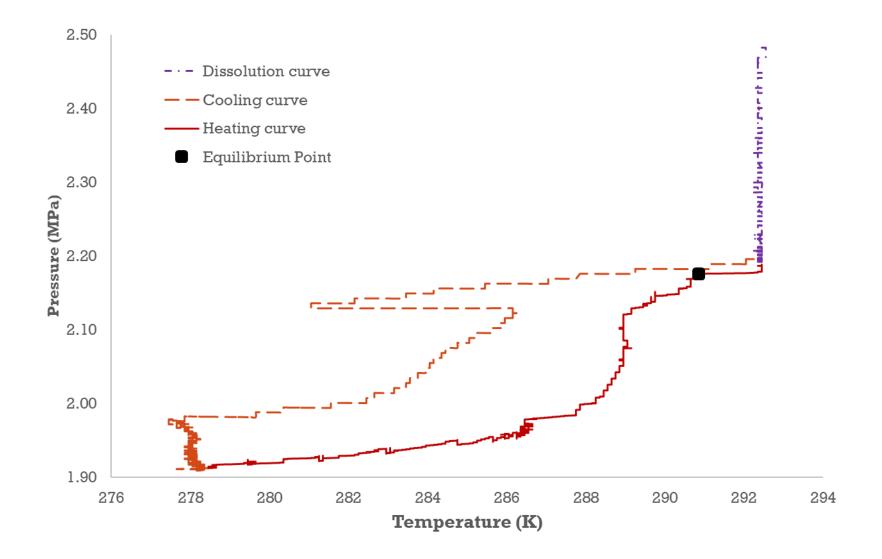
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Small Scale Stirred Tank Reactor

- Phase equilibrium
- Formation Kinetics
 - Induction time
 - Rate of hydrate formation
 - Total gas uptake
- Dissociation Kinetics
- % Water conversion to hydrate

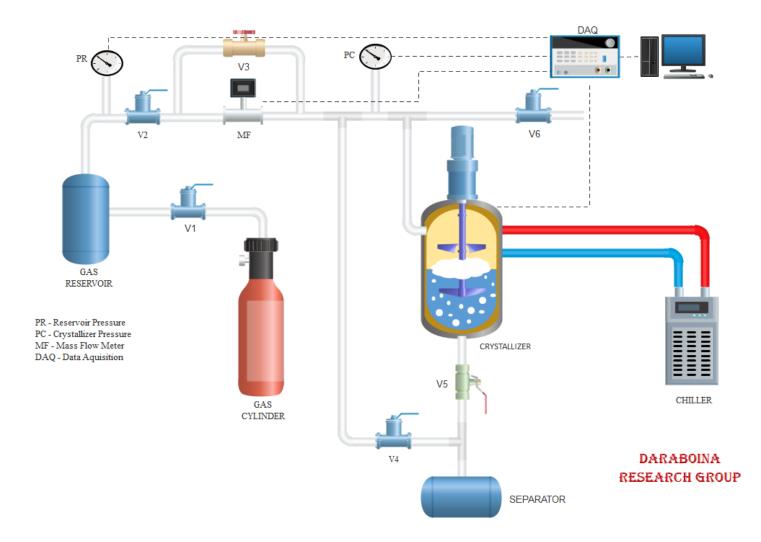


Isochoric Phase Equilibrium Measurement





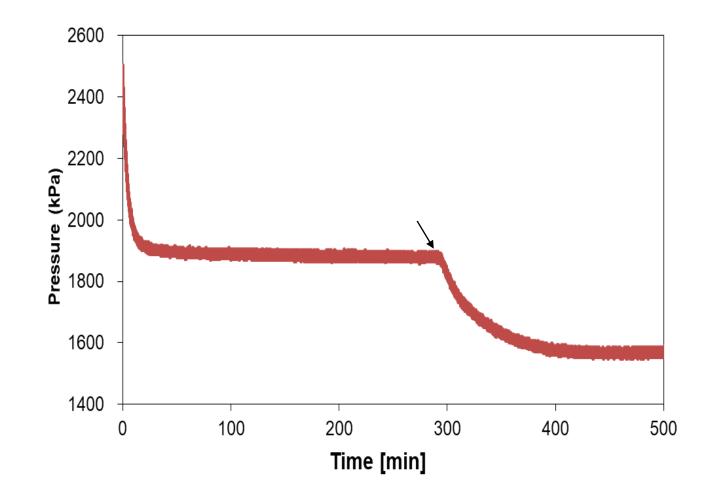
Prototype Reactor



- 4 L Reactor
- Pressure 1000 psi
- Temperature -10 °C to 40 °C

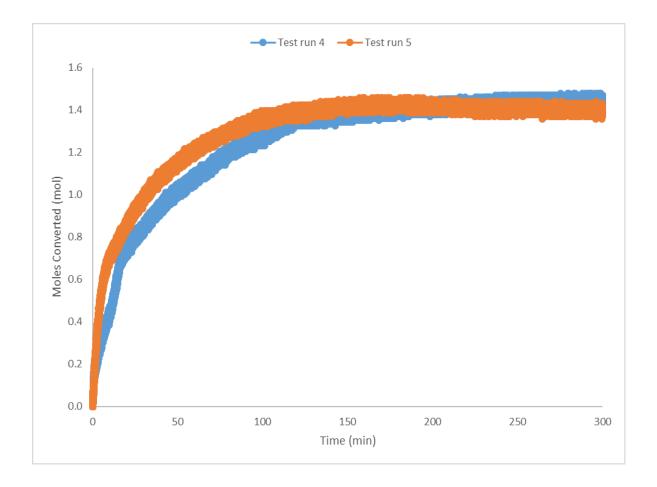


Gas uptake measurement





Hydrate Growth curve



- Experiments with CO₂ at 360 PSI and 2.5 °C
- Repeatability

Summary

- Desalination via Clathrate Hydrate is a sustainable technology
- Need to identify a suitable hydrate former that can increase the operating temperature and enhances hydrate formation kinetics
 - Tetra-n-butyl ammonium bromide testing in progress



Moving forward

- To study kinetic water recovery experiments with different salts and different TBAB concentrations
- Salt rejection study at different concentrations of TBAB
- To optimize of operating conditions for maximum water recovery and salt rejection
- To evaluate OPEX and CAPEX



Process Simulation – Hysys

• Process simulation

- System integration and optimization of the process
- Establish mass and energy balance
- Determine water recoverable through system integration

• Economic analysis

- Sizing and costing of various process equipment
- Analysis on operating costs incurred and determine cost of water



Acknowledgments

Daraboina Research Group